

Implementing potential risk assessment under economic and technical aspects in petroleum production stage

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ABSTRACT

Industries grapple with formidable challenges stemming from uncertainties that not only impede economic growth but also introduce risks in technical realms, impacting operational procedures, performance, and associated services. Addressing prevalent risks in geology, economics, operations, development, and production stages becomes imperative, prompting the implementation of robust risk management and control measures. These measures are vital to ensuring production efficiency, preserving economic values, and conducting a comprehensive risk analysis that influences project outcomes, ultimately guiding investment decisions.

The research at hand aims to delve into the intricate web of factors influencing production performance and to conduct a thorough risk assessment grounded in economic values and production rates, specifically focusing on well X. Employing a holistic approach, the study seamlessly integrates qualitative and quantitative methods, utilizing sophisticated tools such as Nodal Analysis, the material balance equation (MBE), and risk assessment based on net present value (NPV) through the utilization of Crystal Ball software. The overarching goal is to provide a nuanced and comprehensive understanding of the multifaceted dynamics influencing the production of well X.

In summation, the analysis conducted in this study serves as a valuable foundation for informed decision-making processes. By identifying and thoroughly assessing factors that impact production and the economic aspects of well X, the research seeks to mitigate risks during the production stage and guide investment decisions. The amalgamation of qualitative and quantitative methodologies employed in this study not only enriches the depth of understanding but also contributes to a more sophisticated approach to decision-making in the intricate domains of production and investment. Ultimately, the recommendations derived from this study are poised to enhance the resilience of well X in the face of uncertainties, bolstering both its production performance and economic viability.

Key words: Nodal Analysis, Net Present Value, economic evaluations

1 INTRODUCTION

The petroleum industry is a key economic sector, ensuring national energy security, ensuring the economic growth of the country quickly and sustainably, as well as protecting national security and sovereignty at sea. Risks in oil and gas differ from other industries due to their specialized characteristics as well as the technical parameters, which are the foundation, supporting the decision-making process¹⁻³. Therefore, learning about oil and gas and issues related to this field also contributed to the process of developing oil and gas projects. There are several stages of an oil and gas process: Exploration, Appraisal, Development, Production, and Abandonment, which describe a long-life cycle of a petroleum project⁴⁻⁶. Besides, there are many deciding elements in the choice to construct an oil and gas project, making the use of statistical risk assessment difficult. As a result, issues of technical and economic values also have an

impact on the investment decision of the project during the production phase due to the high risks associated with oil and gas^{5,7}.

METHODOLOGY

For each stage of petroleum industry, there are variety of methods to define and evaluate risks such as deterministic, probabilistic and intergrated approach. In this research, with various factors affecting to the production such as technical error, cost overruns, uncertainties in relation to critical variables (infrastructure, production schedule, quality of oil, operational costs, reservoir characteristics,...) and uncertainties in decision-making, therefore, an integrated model was defined so as to analyze technical and economic aspect of an oil well in petroleum production stage^{8,9}. A general workflow that proposed by this research is presented in (Figure 1) and is briefly described as below:

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38 First, the production model is performed to calcu-
 39 late the flowrate of well due to pressure base on Beggs
 40 and Brill correlation and define the operation flowrate
 41 of the Inflow Performance (IPR) and Outflow Perform-
 42 ance (OPR) of production well 1X.

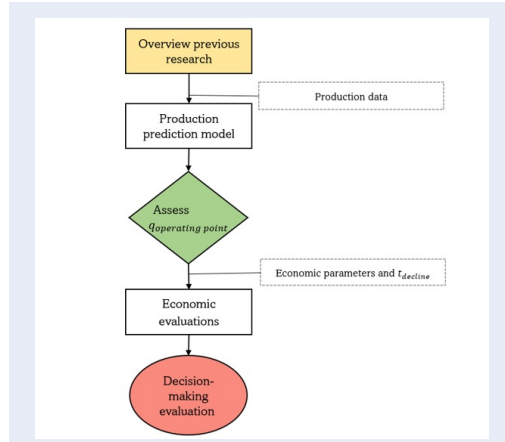


Figure 1: Workflow for the model's calculation

43 • Then, the Economic evaluation is conducted by using
 44 Material Balance Equation (MBE) to calculate the
 45 production rate decline, decline rate and abandon-
 46 ment production. Based on some assumptions, this
 47 provides economic parameters and assists the Risk
 48 analysis model.

49 • After that, the Risk analysis model is performed to
 50 analyze the effects of Net Present Value (NPV) by using
 51 Probabilistic risk assessment approach (PRA).
 52 This workflow is described in detail for each step in
 53 each approach in the next section.

54 **Multiphase flow modeling**

55 The multiphase modeling in this section determines
 56 the relationship of outflow and inflow performance,
 57 flow regime and pressure distribution of the fluid
 58 along the wellbore.

59 This research utilizes Vogel's method for the Inflow
 60 performance calculation for multiphase flow's calcu-
 61 lation 10-12.

62 The indicated a empirical equation applied for two
 63 phase flow, which is described as:

$$\frac{q_0}{q_{max}} = 1 - 0.2 \left(\frac{p_{wf}}{p_b} \right) - 0.8 \left(\frac{p_{wf}}{p_b} \right)^2$$

64 Where q_{max} is the maximum flow rate, q_0 is the initial
 65 flowrate, p_b is the pressure at the bubble point, and
 66 q_{wf} is the pressure at the well flow.

67 For the pressure drop, the correlation is one of the
 68 few correlations capable of handling all flow direc-
 69 tions encountered in oil and gas operations, namely
 70 uphill, downhill, horizontal, inclined and vertical flow
 71 for two phase fluid 12,13. Total pressure gradient is de-
 72 scribed following steps below:

Step 1: Calculate the mixture flow rate

$$q_{mixture} = (B_0 q_{0,sc} B_{w,sc} q_{w,sc}) + \left(B_g \frac{q_{g,sc} - q_{o,sc} R_s}{5800.6408} \right)$$

Step 2: Calculate the mixture specific gravity

$$\gamma_{mixture} = \frac{(\rho_L H_L) + (\rho_G (1 - H_L))}{62.28}$$

Step 3: Calculate the no-slip mixture specific gravity

$$\gamma_{mixture} = \frac{(\rho_L \lambda) + (\rho_G (1 - \lambda))}{62.428}$$

Step 4: Calculate the mixture density

$$\rho_{mixture} = (\rho_L H_L) + \rho_G (1 - H_L)$$

Step 5: Calculate the mixture viscosity

$$\mu_{mixture} = (\mu_L H_L) + \mu_G (1 - H_L)$$

Step 6: Calculate the Reynold's number using no slip
 mixture density and viscosity

$$Re = 124 \times \frac{\rho_{mixture} |V_m| d_{ti}}{\mu_{mixture}}$$

Step 7: Calculate the no-slip friction factor

If $Re \leq 2300$,

$$f_{ns} = \frac{4 \left(\frac{1}{-4 \log_{10} \frac{\epsilon}{d_{ti}}} \right)}{\frac{3.7065 \epsilon}{\left(\frac{5.0452}{Re} \times \frac{\log_{10} d_{ti} 1.1098}{2.8257} \right) + \left(\left(\frac{7.149}{Re} \right)^{0.8981} \right)^2}$$

The ratio of friction factor is calculated using
 Colebrook-White equation:

$$e^S = \frac{f}{f_{ns}}$$

The value of S is governed by following conditions:

$$S = \ln(2.2y - 1.2)$$

If $1 < y < 1.2$, $\ln(2.2y - 1.2)$

And this "s" value is defined as:

$$\frac{\ln(y)}{(-0.00523 + 3.182 \ln(y) - 0.8725 \ln(y)^2 + 0.01853 \ln(y)^4)}$$

Where:

$$y = \frac{\lambda}{H_L(\theta)^2}$$

89 Step 8: Calculate the pressure change due to the hydrostatic head of the vertical component of the pipe.

$$\left(\frac{dp}{dz}\right)_{elevation} = 0.433 \times \gamma_{mixture} \times \sin \theta$$

91 Step 9: Calculate the pressure loss due to friction

$$\left(\frac{dp}{dz}\right)_{friction} = 0.000011471 \times \frac{f_n \frac{f}{f_n} \gamma_{no slip mixture} q_{mixture}^2}{d_{ti}^5}$$

92 Finally, calculate the total pressure gradient from the pressure change due to the hydrostatic head of the vertical component of the pipe and pressure loss due to friction.

$$\left(\frac{dp}{dz}\right) = \left(\frac{dp}{dz}\right)_e + \left(\frac{dp}{dz}\right)_f$$

96 **Economic evaluations**

97 For petroleum economic evaluation, the worth of petroleum qualities, quantities of petroleum commodities, and corresponding economic life are determined using Net Present Value and related computations. Quantities of producible oil and gas up to the economic life reserve are quantified. Almost all economic appraisals of petroleum properties are purely based on decline curve analyses, with no consideration given to material balance parameters and their implications on reservoir pressures and decreasing rates, as well as their effects on value¹⁴.

98 Material Balance Equation is utilized to support the important pressure-time relationship in addition to the underground extraction and reservoir depletion (Figure 2). Therefore, the forecast of good production would be related with well deliverability¹⁵.

99 This section utilizes material balance equation's calculation to calculate the cumulative oil production, abandonment time and define oil and gas production forecast, where the N_p^1 and G_p^1 is the cumulative oil and gas production at the beginning of the interval and ΔN_p^1 and ΔG_p^1 is the incremental cumulative oil and gas production.

$$\Delta N_p^1 = \frac{1 - \bar{\phi}_n N_p^1 - \bar{\phi}_g G_p^1}{\bar{\phi}_n + \bar{R} \bar{\phi}_g}$$

120 and

$$\Delta G_p^1 = \Delta N_p^1 \bar{R}$$

121 From these tasks, the Production decline profile can be obtained to support the economic calculations such as Net present value, which is a financial statistic

124 that attempts to represent the total worth of the investment opportunity.

125 The research can generate the economic calculation to obtain the NPV value using the fomular below:

$$NPV = \sum_{n=1}^N \frac{C_n}{(1+r)^n}$$

128 Then, the Net present value (NPV) can also be determined by calculating the difference between the Present Value (PV) after a time period of investment and the initial amount invested, where the Present Value "PV" after time "t" given a rate of return "r" can be calculated.

134 **Risk analysis modeling**

135 The risk analysis model in this research applied Crystal Ball software to analyze the Net Present Value using the Probabilistic approach (Figure 3).

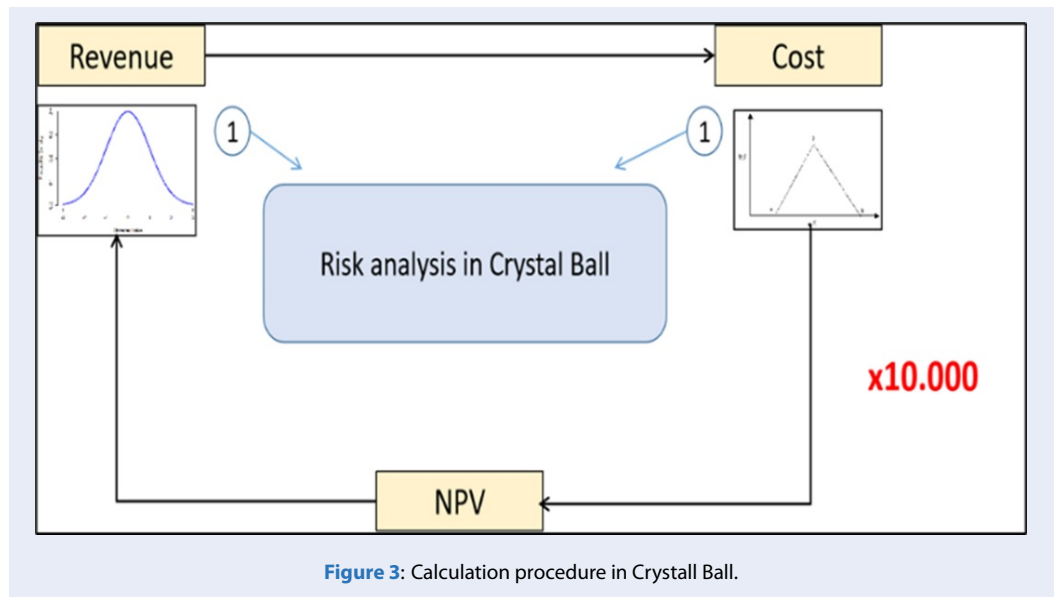
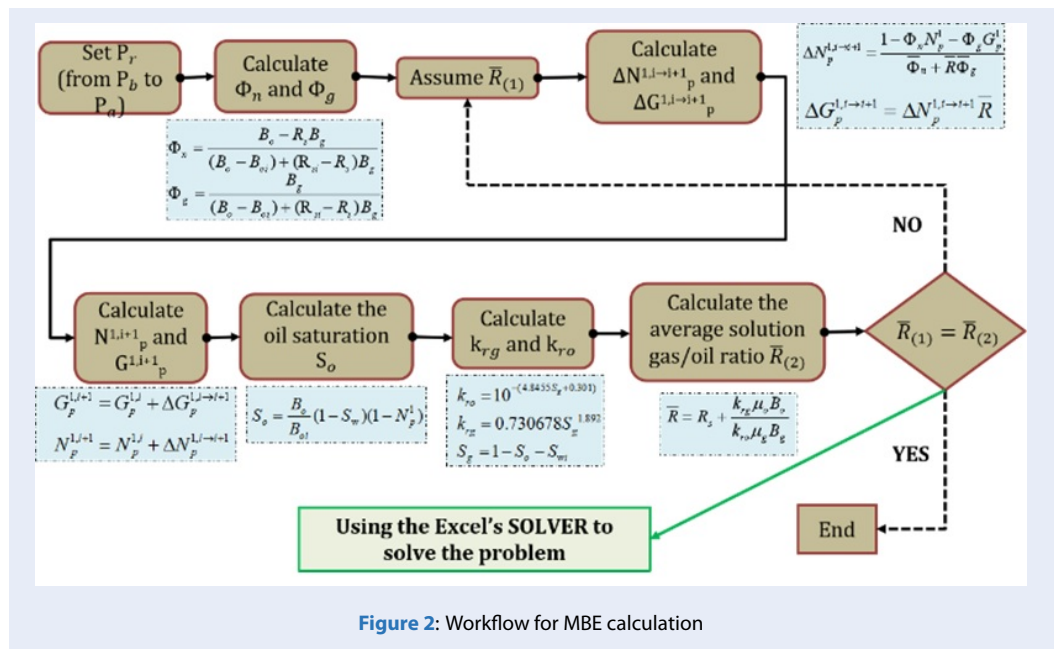
136 Sensitivity analysis (SA) is an important component for determining which model variables will have the greatest impact on the outcome. The impact of a reservoir property is defined in the SA as the difference (absolute value) between the NPV evaluated at the minimum and maximum value of the property (NPV).

145 Besides, sensitivity analysis (SA) is a vital assessment component for determining which variables will have the greatest impact on the outcomes. The impact of a reservoir property is defined in the SA as the difference (absolute value) between the NPV evaluated at the minimum and maximum value of the property (NPV).

152 **RESULTS**

153 Input data of this research is collected from book and references in petroleum engineering, a production oil well with multiphase flow including oil, gas and water. Some of the main assumptions are used in this work and described in this workflow:

- The well is vertical. 158
- Fluid flow in the tubing is pseudo-steady state and one dimension from bottom-hole to wellhead. 159-161
- The temperature of fluid distributes linearly with depth from bottom-hole to wellhead. 162-163
- The cost is hypothesized to perform the economic calculation 164-165



166 **Production rate calculation results and sen-**
 167 **sitivity analysis**

168 The Nodal Analysis, from combining the IPR and
 169 OPR curves reveals the operating point at which a
 170 well can produce at a given pressure and rate (Fig-
 171 ure 4). The result for the operating production rate is
 172 to obtain at the $q_{operating} = 965,7759675$ stb/day when
 173 pressure is at 3419,497098 psia due to the relationship
 174 between IPR and OPR, shown in the figure below.

175 With variation of reservoir pressure, the well perfor-
 176 mance is described in the (Figure 5). Sensitivity any-

167 sis in (Figure 6), it demonstrates the influence of well-
 168 head pressure has a great impact on the performance
 169 of the production rates.

170 Besides, Systems Nodal Analysis can be used to inves-
 171 tigate the effects of a wide range of circumstances on
 172 oil and gas well performance.

173 Well head pressures are varied from 450 psia to 2000
 174 psia, which means from the operating point until the
 175 point where the OPR and IPR lines no longer intersec-
 176 t.

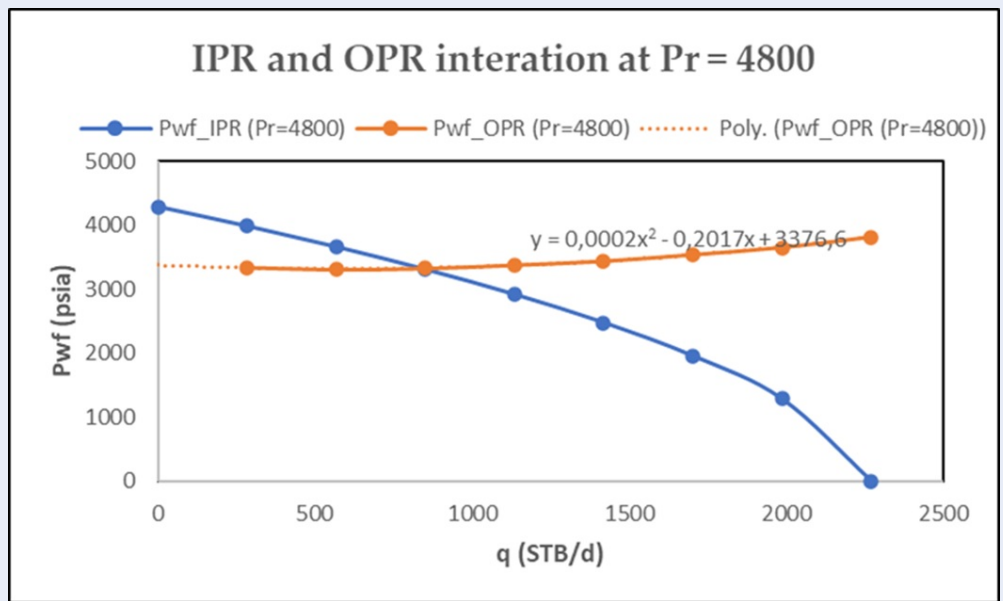


Figure 4: IPR And OPR curve at the reservoir pressure

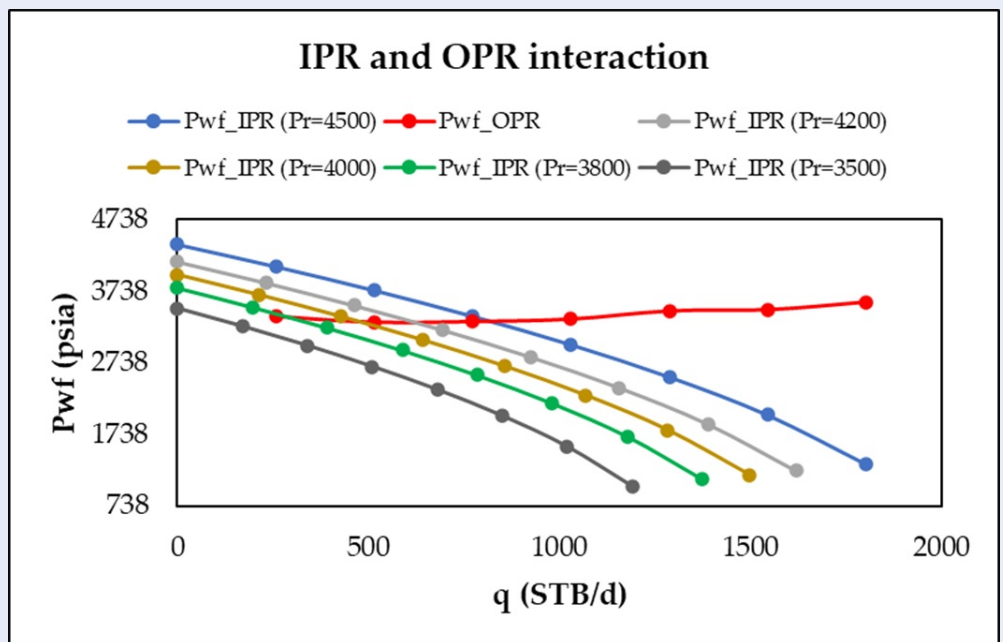


Figure 5: Operating q point with variation of reservoir pressure based on IPR and OPR in Excel.

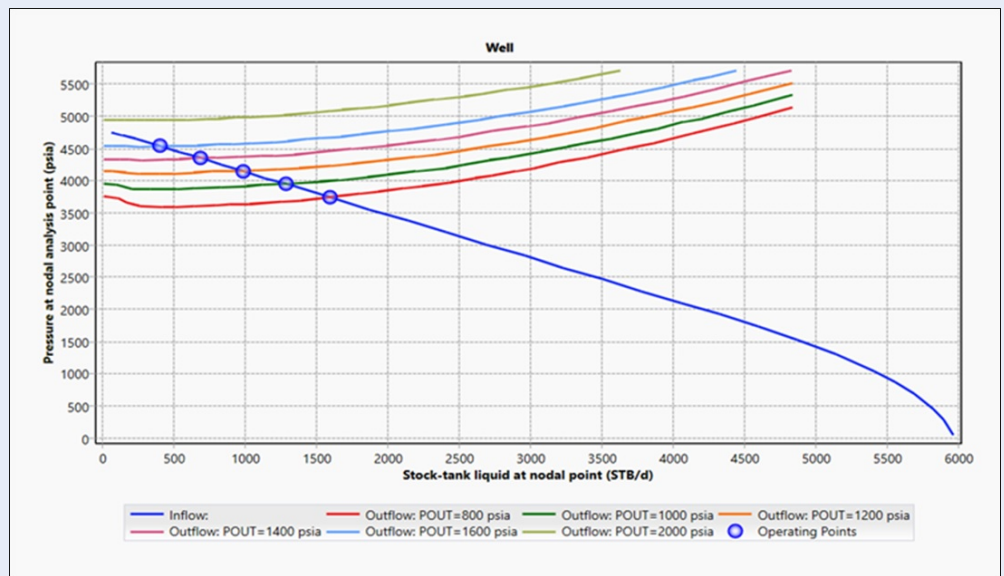


Figure 6: Variation of well head pressure in IPR and OPR plot

187 The Nodal analysis evaluates the behavior and effect of
 188 the components that make up the production system,
 189 perforation density and size, formation fluid charac-
 190 teristics, and fluid production rates. Besides, the wa-
 191 ter cut ranged from 15% up to 80% so as to observe
 192 the effect of this parameter on the IPR.
 193 From the result from the software, it can be seen that
 194 the 80% of water cut received significant impact to the
 195 well performance (Figure 7).

196 **Economic evaluation and risk analysis**
 197 **model**

198 From the Production decline profile, it can be ob-
 199 served the well production problems as well as the well
 200 performance and life of a project based on production
 201 data. The outcome of production rates gradually de-
 202 creased year by year with production from 736.139 to
 203 137.735 stb/day during 8 years (Figure 8).

204 Figure 9 showed that the flow value continuously de-
 205 clines in both days and years with total CAPEX and
 206 OPEX expenditures totaling \$16.770.276,818 at an oil
 207 price of 70\$/barrel and annual operating costs of ap-
 208 proximately \$545,000.

209 The results from the above diagram indicated the net
 210 present value is \$37.990.032,443 from production de-
 211 cline profile with respect to the time and economic
 212 assumptions (Figure 10).

213 For risk analysis in Crystal Ball, the concept is the
 214 revenue focusing on normally distributed with error
 215 +10% or -10% and cost according to triangle distribu-
 216 tion with min, likely and max cases to calculate NPV

217 value based on analysis in Crystal Ball (Figure 11).
 218 The simulation followed the normal distribution to
 219 compute the predicted NPV value based on the speci-
 220 fied input distribution. The graph shows that the NPV
 221 value based on probability ranges from \$25.000.000 to
 222 \$55.000.000 relying on normal distribution.

223 When the model set the revenue limit, the likelihood
 224 of achieving an NPV value of \$39.990.032,443 reaches
 225 up to 57.85%. Around 48.89% of this model failing to
 226 achieve this value, the negative NPV values might be
 227 between \$25.000.000,000 to \$40.000.000,000 accord-
 228 ing to the NPV's graph following the normal distribu-
 229 tion (Figure 12).

230 Besides, when the model sets the revenue limit
 231 with the certainty at 80%, the NPV value can
 232 be achieved from between over \$31.541.593,720 to
 233 \$46.526.542,491 (Figure 13).

234 In this sensitivity analysis section, based on the dia-
 235 gram, the impact of revenue on NPV is 87.1% while
 236 the cost only takes up about 12.9%. Besides, with the
 237 support of sensitivity analysis, the influences of rele-
 238 vant parameters are presented due to the simulation
 239 analysis.

240 **DISCUSSION**

241 Establishing an effective methodology proves to be a
 242 formidable challenge when addressing the input char-
 243 acteristics directly associated with a virtual model uti-
 244 lizing MBE and NPV. Consequently, the resulting
 245 output aims to illustrate the relationship between IPR

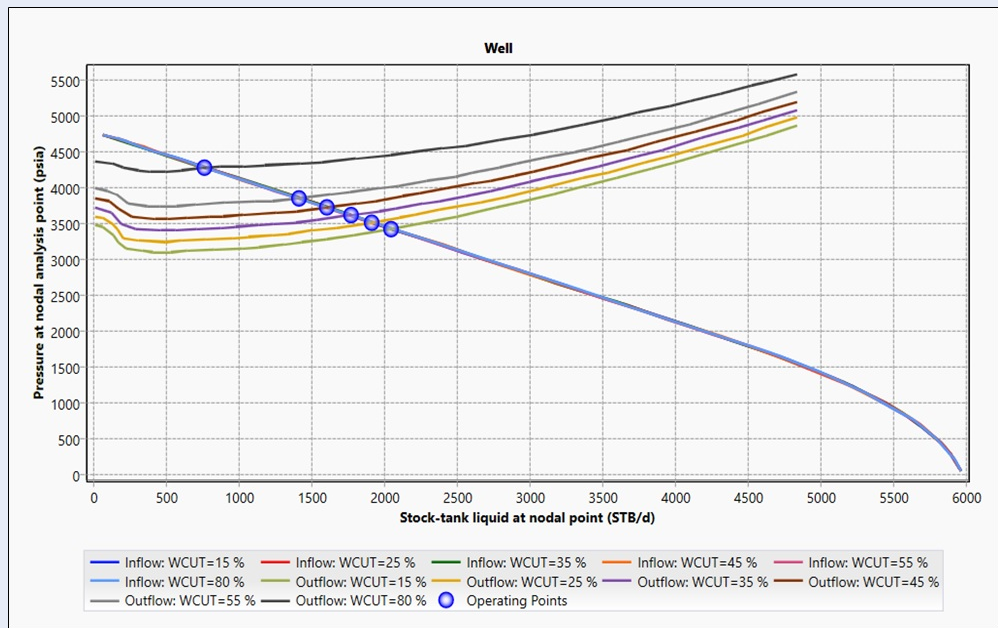


Figure 7: Variation of water cut in IPR and OPR plot

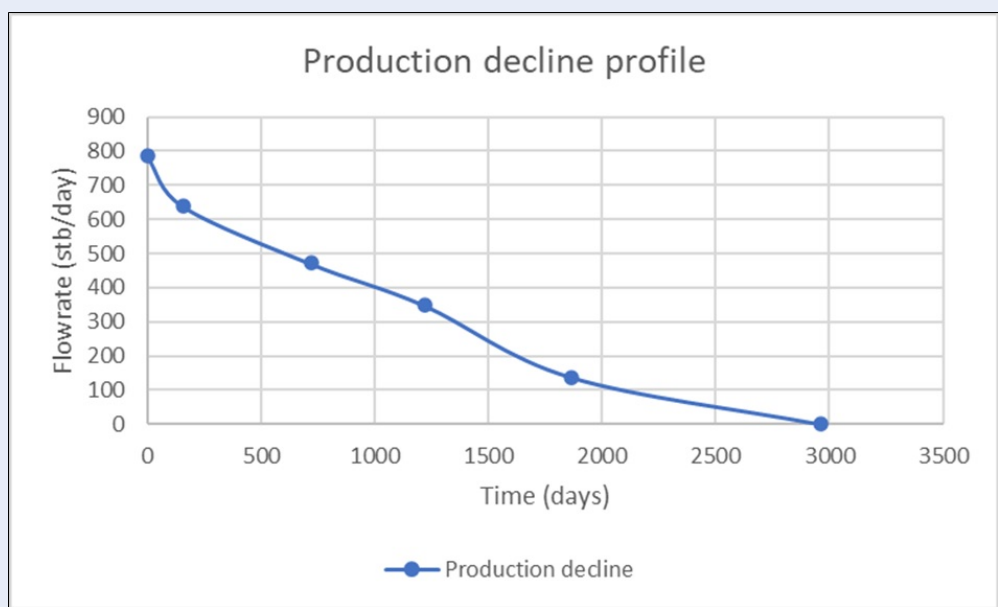


Figure 8: Production decline profile vs. flowrate

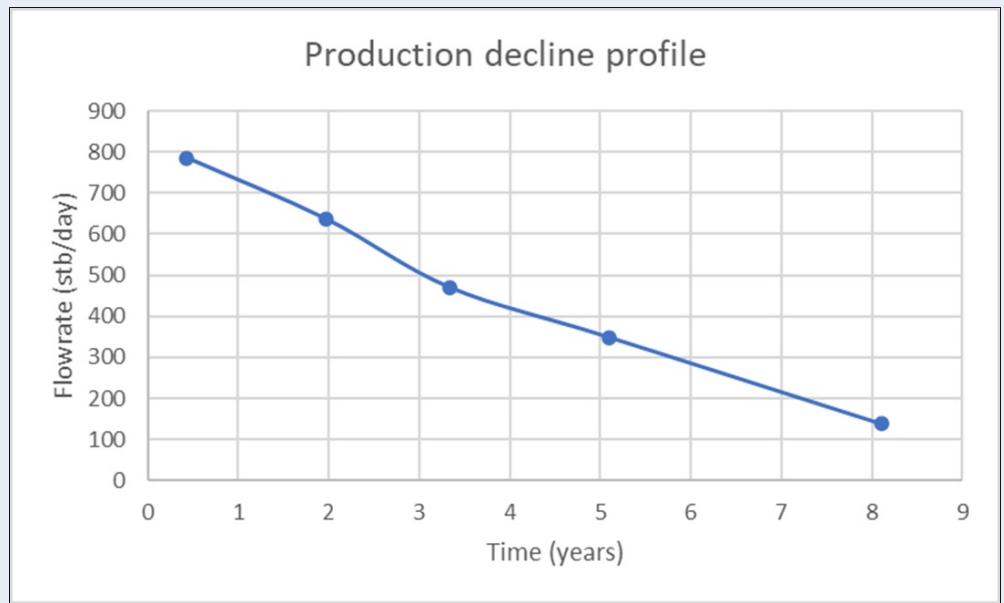


Figure 9: Production decline profile of Oil Well X due to years

Year	Flowrate	Revenue (\$/day)	Revenue (\$/year)	Cost of oil (\$/year)	Tax
0,4	786,1	\$55.029,7	\$20.085.848,2	\$3.347.641,4	\$2.008.584,8
2,0	638,0	\$44.663,1	\$16.302.026,4	\$2.717.004,4	\$1.630.202,6
3,3	470,9	\$32.965,2	\$12.032.288,9	\$2.005.381,5	\$1.203.228,9
5,1	348,6	\$24.398,6	\$8.905.496,1	\$1.484.249,3	\$890.549,6
8,1	137,7	\$9.641,4	\$3.519.128,6	\$586.521,4	\$351.912,9

Figure 10: Result for economic evaluation due the the production decline analysis

246 and OPR through a plotted graph. However, the rep-
 247 resentation faces additional limitations attributed to
 248 imperfections in the imperial diagram. These con-
 249 straints pose obstacles in achieving a more nuanced
 250 and accurate portrayal of the relationship between
 251 IPR and OPR. The imperfections within the imper-
 252 rial diagram contribute to the challenges of compre-
 253 hensively capturing the dynamics involved in the in-
 254 terplay between input characteristics and their corre-
 255 sponding output results. Mitigating these limitations
 256 becomes imperative for refining the reliability and
 257 precision of the virtual model, ensuring a more thor-
 258 ough depiction of the complex relationships within
 259 the IPR and OPR framework. Moreover, economic
 260 evaluation and risk analysis model with NPV at P50
 261 and P80 of Crystal Ball’s analysis are just simulation
 262 analysis, so that still more limitation.

CONCLUSIONS

263 In summary, the research has achieved objectives as
 264 an integrated model for predicting production rate,
 265 economic evaluations, and risk analysis model in the
 266 production stage. The model can be applied to pro-
 267 duction wells, with black-oil models with empirical
 268 correlations.

269 This procedure can be used to the preliminary peri-
 270 od of the project or production stage to support the
 271 decision-making process and define the production
 272 forecast.

273 The risk analysis model using the Crystal Ball software
 274 and a visualized model has been introduced to evalu-
 275 ate the risk for the decision-making process.

276 Besides, the sensitivity analysis evaluated the effects
 277 of pressure, and water cut after defining the operating
 278

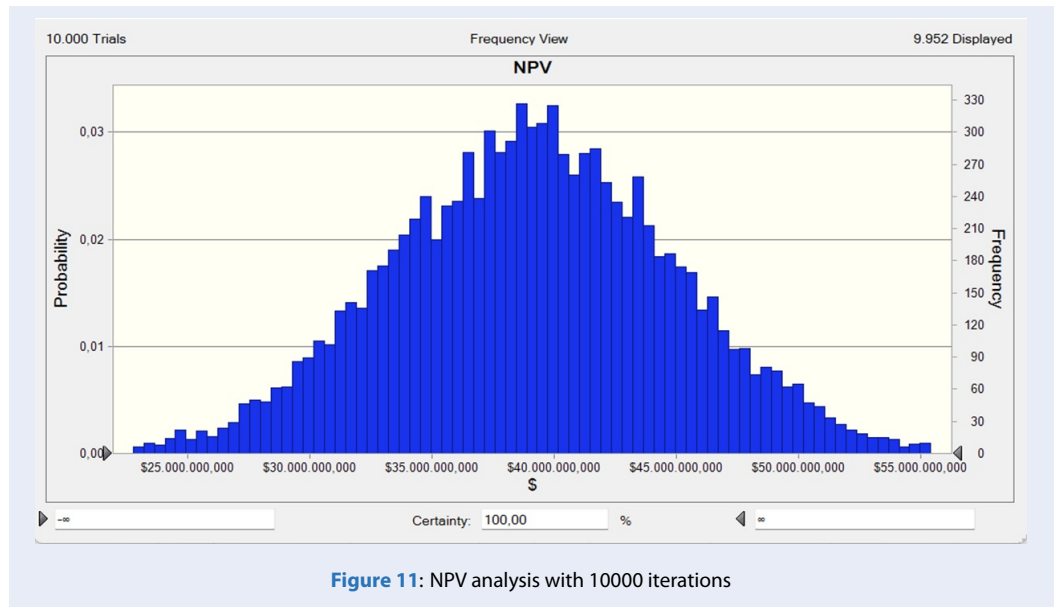


Figure 11: NPV analysis with 10000 iterations

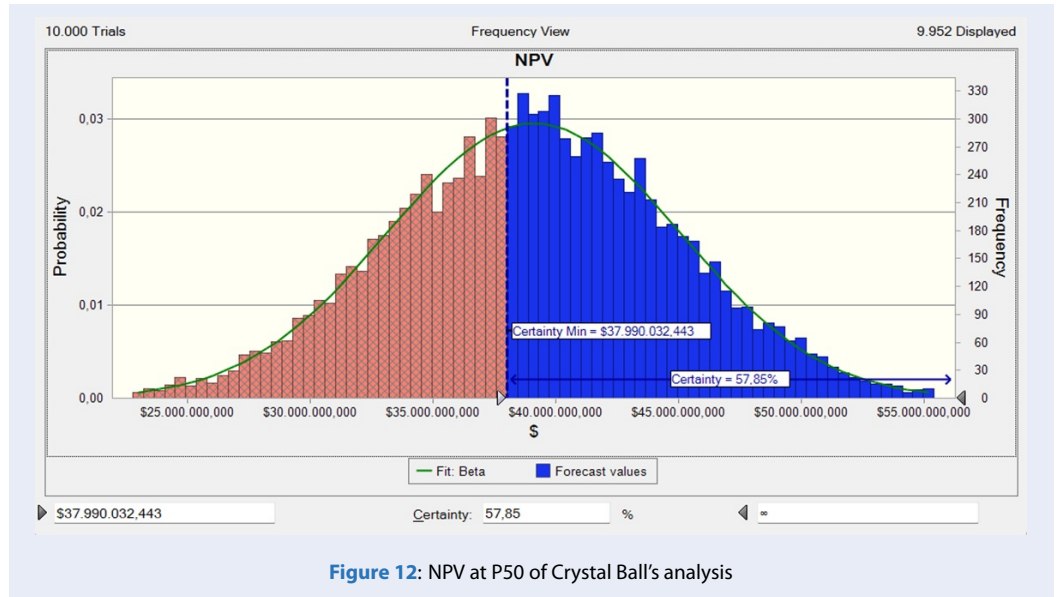


Figure 12: NPV at P50 of Crystal Ball's analysis

279 point due to the relationship of IPR and OPR from
 280 Nodal Analysis along the wellbore. The economic
 281 evaluations also determine the NPV value and the risk
 282 analysis, which assist in the decision-making process
 283 of the project.

284 **ACKNOWLEDGEMENTS**

285 We acknowledge the support of time and facilities
 286 from Ho Chi Minh City University of Technology
 287 (HCMUT), VNU-HCM for this study.

ABBREVIATIONS

- q_o is oil production rate, stb/day.
- q_{max} is the maximum flow rate, stb/day.
- p_{wf} is the pressure at the well flow, psia.
- p_b is the pressure at the bubble point, psia.
- $q_{mixture}$ is the mixture flowrate.
- B_o is the oil formation volume factor, rb/stb.
- B_g is the gas formation volume factor, rb/bbl.
- S is the skin factor.
- $\gamma_{mixture}$ is the mixture specific gravity.
- $\rho_{mixture}$ is the mixture density.
- ρ_L is the density of liquid.

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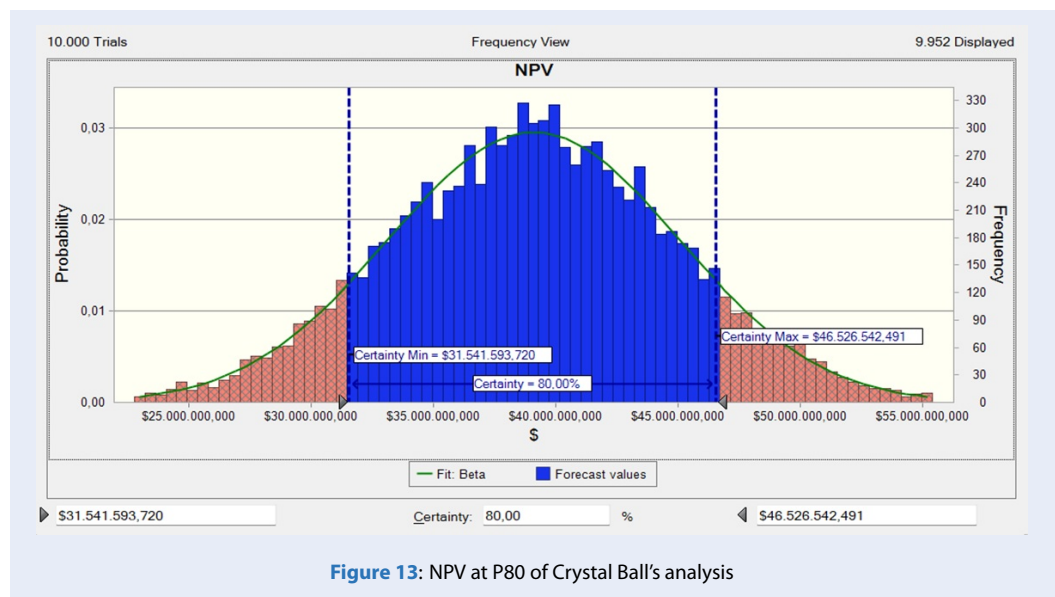


Figure 13: NPV at P80 of Crystal Ball's analysis

300 ρ_G is the density of gas (lbm/[ft]³).
 301 d_{ti} is the inner tubing diameter, in.
 302 λ is the the input liquid content.
 303 V_m is volume of mixture associated with 1 stb of oil,
 304 [ft]³.
 305 $\mu_{mixture}$ is the mixture viscosity (cp).
 306 Re is the Reynold's number.
 307 $H_L(\theta)$ is the liquid hold-up.
 308 f is the friction factor, dimensionless
 309 f_{ns} is no-slip friction factor.
 310 $\frac{f}{f_{ns}}$ is the ratio friction factor.
 311 ψ is the the liquid holdup inclination correction fac-
 312 tor.
 313 $\left(\frac{dp}{dz}\right)_{elevation}$ is the pressure change due to the hydro-
 314 static head of the vertical component of the pipe.
 315 $\left(\frac{dp}{dz}\right)_{friction}$ is the pressure loss due to friction.
 316 N_p^1 and G_p^1 is the cumulative oil and gas production at
 317 the beginning of the interval.
 318 ΔN_p^1 and ΔG_p^1 is the is the incremental cumulative
 319 oil and gas production.
 320 PRA is Probabilistic risk assessment approach.
 321 IPR is Inflow Performance Relationship.
 322 OPR is Outflow Performance Relationship.
 323 NPV is the Net Presen Value.
 324 SA is the Sensitivity Analysis.
 325 MBE is the Matereial Balance Equation.

326 COMPETING INTERESTS

327 We declares no any conflicts of interest to all.

CREDIT AUTHOR STATEMENT

328
 329 **Thong N.H.and Quynh P.N.P.** Conceptualization;
 330 Methodolody; Data; Analysis; Writingg – Review &
 331 Editing. **Thong.N.H.** Supervision. Both **Thong N.H.**
 332 and **Quynh P.N.P.** contributed equally and have the
 333 right to list their name first for this article.

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Ứng dụng đánh giá rủi ro dưới khía cạnh kinh tế và kỹ thuật trong giai đoạn khai thác dầu khí

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TÓM TẮT

Các ngành công nghiệp đối mặt với những thách thức đáng kể xuất phát từ sự không chắc chắn không chỉ làm chậm quá trình tăng trưởng kinh tế mà còn đưa ra những rủi ro trong lĩnh vực kỹ thuật, ảnh hưởng đến quy trình vận hành, hiệu suất và các dịch vụ liên quan. Việc đối mặt với rủi ro phổ biến ở các giai đoạn địa chất, kinh tế, vận hành, phát triển và sản xuất trở nên cấp bách, thúc đẩy việc triển khai các biện pháp quản lý và kiểm soát rủi ro mạnh mẽ. Những biện pháp này là quan trọng để đảm bảo hiệu suất sản xuất, bảo toàn giá trị kinh tế và thực hiện một phân tích rủi ro toàn diện ảnh hưởng đến kết quả dự án, từ đó hướng dẫn quyết định đầu tư.

Nghiên cứu này nhằm làm rõ mạng lưới phức tạp của các yếu tố ảnh hưởng đến hiệu suất sản xuất và thực hiện đánh giá rủi ro kỹ lưỡng dựa trên giá trị kinh tế và tỷ lệ sản xuất, tập trung cụ thể vào giếng X. Sử dụng một phương pháp tiếp cận toàn diện, nghiên cứu tích hợp cả phương pháp định tính và định lượng, sử dụng các công cụ như Phân tích Nodal, phương trình cân bằng vật liệu (MBE), và đánh giá rủi ro dựa trên giá trị hiện tại ròng (NPV) thông qua việc sử dụng công cụ Crystal Ball. Mục tiêu tổng thể là cung cấp các kiến thức để nhận diện đa chiều ảnh hưởng đến sản xuất giếng X.

Tóm lại, phân tích được thực hiện trong nghiên cứu này đóng vai trò như một nền tảng cơ sở cho việc đưa ra quyết định. Bằng cách xác định và đánh giá kỹ lưỡng các yếu tố ảnh hưởng đến sản xuất và khía cạnh kinh tế của giếng X, nghiên cứu nhằm giảm thiểu rủi ro trong giai đoạn sản xuất và hướng dẫn quyết định đầu tư. Sự kết hợp của phương pháp định tính và định lượng được áp dụng trong nghiên cứu này không chỉ làm phong phú sâu sắc kiến thức mà còn đóng góp vào một phương pháp đưa ra quyết định chắc chắn hơn trong các lĩnh vực phức tạp của sản xuất và đầu tư. Cuối cùng, các khuyến nghị xuất phát từ nghiên cứu này được kỳ vọng sẽ tăng cường sự linh hoạt của giếng X trước sự không chắc chắn, nâng cao cả hiệu suất sản xuất và khả năng kinh tế của nó.

Từ khóa: Phân tích Nodal, giá trị hiện tại ròng (NPV), đánh giá kinh tế

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