

Enhanced efficiency MnO₂-Promoted Pt catalyst for VOCs oxidation

Khong Manh Hung*, Tran Van Hien, Ha Quoc Bang

ABSTRACT

One of the leading causes of air pollution, volatile organic compounds (VOCs) pose a severe danger to both the environment and human health. In heat or light, catalytic oxidation has been recognized as a promising and successful approach for treating VOCs. Due to their affordability and environmental friendliness, manganese-based oxides are one of the most competitive and acceptable choices for the catalytic destruction of VOCs. In this study, we disperse Pt on MnO₂ with trace Pt loadings of 0.5, 1, and 1.5 wt% to control the interaction of Pt-MnO₂ (MnO₂ = manganese oxide). In comparison to MnO₂, the Pt-MnO₂ catalyst exhibits higher VOCs oxidation performance due to its higher Brunauer-Emmett-Teller surface area, more active lattice oxygen, increased oxygen vacancy activating increased dioxygen molecules, more exposed Pt atoms, and noninternal diffusion of mass transfer. Among all the platinum samples created with varying mass ratios, the Pt-MnO₂ sample demonstrates the best characteristic characteristics as well as catalytic activity. The specific surface area of Pt-MnO₂ is 108.74 m²/g. The Pt-MnO₂ catalyst can totally convert Toluene into CO₂ and H₂O at a lower temperature of just 190 C while maintaining great stability for 600 minutes. Under conditions of high space velocity, the Pt-MnO₂ catalysts' performance in oxidizing VOCs is steady, indicating tremendous promise for real-world use. This research shows that a Pt-dispersed MnO₂ catalyst is superior to a MnO₂ catalyst for the oxidation of VOCs, offering universally significant advice for the interaction of metals with supports and the control of interfaces during oxidation processes. The results suggest that the synthesized Pt-MnO₂ material has a comparatively strong capacity to oxidize VOCs at low temperatures and a high stability, and that it can be developed and scaled up to a wider application scale.

Key words: Manganese oxide, Platinum, Toluene, catalytic oxidation, VOCs

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INTRODUCTION

The burning of fossil fuels, the volatilization of liquid fuels and solvents, and the emissions from chemical plants are the primary causes of VOCs emissions. In addition to being poisonous, carcinogenic, and mutagenic to humans, VOCs also threaten air quality by depleting the ozone layer and acting as precursors to photochemical smog. Thus, it is crucial to choose efficient VOCs pollution reduction strategies¹⁻³. Diverse control strategies, including combustion, photocatalytic oxidation, adsorption methods, membrane separation, biotechnology, and catalytic oxidation, have been developed to limit the emissions of VOCs⁴⁻⁷. Catalytic oxidation has been regarded as one of the most promising techniques due to its high efficiency, energy conservation, and environmental friendliness^{8,9}. The catalyst is often the most critical component in the low-temperature catalytic oxidation of VOCs. Noble metal-based catalysts are very effective in removing VOCs from the environment. However, their widespread use was hampered by their high cost, resource scarcity, and poor thermal

stability. Contrarily, transition metal-based catalysts have gained popularity due to their inexpensive cost, strong thermal stability, and excellent oxygen storage capacity^{10,11}.

Transition metal oxide catalysts have demonstrated considerable potential in various applications owing to their advantageous characteristics such as cost-effectiveness, resistance to poisoning, and resistance to sintering^{12,13}. Therefore, it is imperative to utilize transition metal oxide-based catalysts that exhibit elevated catalytic activity towards VOCs at reduced temperatures. There has been a growing interest in studying Co₃O₄, CeO₂, and MnO₂ in the past few years due to their well-defined and controlled nanostructures¹⁴⁻¹⁶. One notable example is MnO₂, which exhibits adjustable atomic valence states and crystalline phases. The catalyst based on MnO₂ is widely recognized for its high efficiency in converting ozone and its notable ability to adsorb VOCs and effectively activate oxygen at low temperatures¹⁷⁻²⁴. According to the study conducted by Li et al., it was observed that α-MnO₂ exhibited a higher preference for the oxida-

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tion of acetaldehyde and benzene to CO_2 compared to $\gamma\text{-MnO}_2$ and $\beta\text{-MnO}_2$. The phenomenon above can be ascribed to the favorable adsorption capacity and notable oxygen migration ability exhibited by $\alpha\text{-MnO}_2$. In a study conducted by Liang et al., it was shown that MnO_2 with unique crystalline phases displayed varying levels of catalytic activity in the oxidation of CO. Specifically, $\delta\text{-MnO}_2$, and $\alpha\text{-MnO}_2$ exhibited superior catalytic performance compared to $\gamma\text{-MnO}_2$ and $\beta\text{-MnO}_2$ ²⁴.

In recent years, numerous researchers have endeavored to augment the catalytic efficacy of catalysts based on MnO_2 by integrating additional metal species^{25,26}. Several bimetallic catalysts, including Ag-Mn, Ni-Mn, and Ru-Mn, were synthesized specifically to degrade VOCs²⁷⁻³⁰. The introduction of an additional metal element not only influences the microstructural characteristics of MnO_2 , such as specific surface area, crystallinity, and shape but also leads to synergistic effects that enhance the catalytic performance. The production of oxygen vacancies is facilitated by the interfacial active sites seen in both metal and metal oxide materials³¹. The proper cycling of dynamic oxygen species on the catalyst surface is critical in achieving deep oxidation of VOCs³². Moreover, it is widely acknowledged that Pt-based catalysts are the most preferred catalysts for the oxidation of VOCs at low temperatures^{33,34}. In their study, Zhang et al.³⁵ employed Pt/ MnO_2 as a catalyst for the oxidation of toluene. The results indicated that Pt/ MnO_2 exhibited favorable catalytic activity under low-temperature conditions. The robust intermolecular interactions observed between manganese (Mn) and platinum (Pt) have been found to significantly augment the redox capability of catalysts composed of Pt/ MnO_2 . Thus, there is a strong demand for developing a Pt/ MnO_2 catalyst that exhibits exceptional activity to enhance the oxidation of VOCs.

In this study, we provide a hydrothermal combine approach combined with impregnation methods for synthesizing Pt/ MnO_2 . Our objective is to investigate the impact of the cation complex on the toluene oxidation process by altering the weight percentage of Pt at low temperatures. This study presents a proficient approach toward the component engineering of platinum and transition-metal oxides and their subsequent utilization in catalytic applications for the oxidation of toluene.

EXPERIMENT METHODS

Material

$\text{MnSO}_4 \cdot \text{H}_2\text{O}$, standard benzene solution, KMnO_4 , Polyvinylpyrrolidone (PVP), Sodium Citrate

($\text{Na}_3\text{C}_6\text{H}_5\text{O}_7$), and L-Ascorbic acid were purchased from Xylong Ltd. Standard gas cylinders H_2 , Ar, He, N_2 , and O_2 are also used of domestic origin.

Preparation of catalysts

Synthesis of Manganese oxide MnO_2 TN

The experimental procedure involved the addition of 0.1 moles of potassium permanganate (KMnO_4) to a volume of 30 milliliters of distilled water. Subsequently, 0.15 moles of manganese sulfate (MnSO_4) solution was gradually added to the solution above. The resulting mixture was subjected to a heating process at ambient temperature for 4 hours, followed by transfer to an autoclave and further heating at 160 degrees Celsius for 3 hours. The liquid undergoes filtration, washing, and drying processes at a temperature of 80 °C on a nightly basis. The final product under consideration is manganese dioxide (MnO_2 TN) in its thermodynamically stable state.

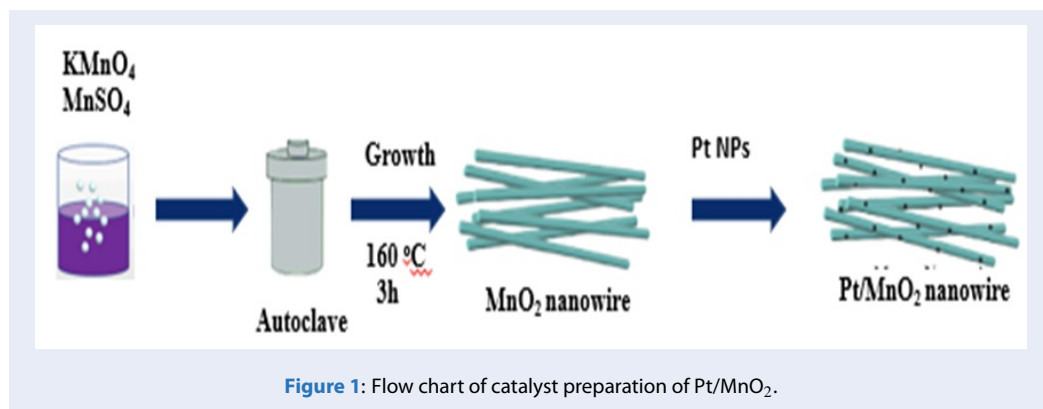
Synthesis of Manganese oxide MnO_2 TN

The impregnation approach is utilized to carry Pt on top of MnO_2 . To prepare solution A, 68 mg of PVP powder and 0.18 g of Sodium Citrate were dissolved in 100 ml of distilled water. To obtain solution B, 16mg of $\text{H}_2\text{PtCl}_6 \cdot 6\text{H}_2\text{O}$ was dissolved in 10 milliliters of pure water. Gradually incorporate solutions B and A into the mixture and agitate for 5 minutes to obtain solution C. To obtain solution D, 10 ml of distilled water should dissolve 108 milligrams of ascorbic acid. The process of creating a Pt colloidal solution involves the gradual addition of D into solution C, followed by continuous stirring for a duration of 2 hours.

A solution containing 0.5 grams of MnO_2 dispersed in 50 milliliters of distilled water was exposed to ultrasonic vibration for 15 minutes. Subsequently, this solution was introduced into the Pt colloidal solution. The mixture should be stirred continuously and subjected to a temperature of 80 °C for a duration of 2 hours. The resultant product underwent filtration, followed by washing with distilled water and ethanol, and afterward underwent overnight drying at a temperature of 80 °C.

Furthermore, samples of 0.5Pt/ MnO_2 and 1.5Pt/ MnO_2 (with a mass percentage of Pt in the catalyst mixture of 0.5%w and 1.5%w, respectively) were synthesized using the same procedure described above. The only distinguishing factor between these entities is the variation of the precursor H_2PtCl_6 's mass.

The synthesis process of Pt/ MnO_2 is clearly illustrated in Figure 1.



Characterization of catalyst

The present work focused on analyzing catalyst morphology and microstructure by utilizing a scanning electron microscope (SEM) model Hitachi S-4800, manufactured in Japan. The chemical compositions and metal concentrations of catalysts were studied using a scanning electron microscope with an X-ray microprobe analyzer (EDS) spectrometer. The held samples were subjected to X-ray diffraction (XRD) analysis using D8 Advance Bruker equipment. The synthetic materials' Fourier Transform Infrared (FTIR) spectrum was examined in the wavenumber range of 400 to 4000 cm⁻¹ using a reflection technique on a Bruker Tensor II instrument.

Measurement of catalytic activity

A micro-reactor system was employed for the remediation of benzene. The gaseous toluene was generated by adding nitrogen gas into liquid benzene via bubbling. Subsequently, it was subjected to a combination of N₂ and O₂. The flow rate of the entire mixture of reactants was established at 50 mL/min. Once the benzene concentration at the intake reached a steady state of 6,000 parts per million (ppm) and the gas hourly space velocity (GHSV) reached 11,000 h⁻¹. A quantity of 0.1 grams of each catalyst was placed at the center of a 60-centimeter-long reactor with a diameter of ¼ inch. The contents of CO₂ and benzene were determined by employing an online Focus-Thermo Scientific gas chromatograph equipped with a thermal conductivity detector (TCD) and a flame ionization detector (FID).

The benzene conversion ($X_{Toluene}$, %) was calculated using the following equation

$$X_T = \frac{C_T^1 - C_T^2}{C_T^1} \times 100 \quad (1)$$

Whereas:

X_T : Toluene conversion (%)

C_T^1 : Toluene concentration of inlet flow at a temperature T (ppm);

C_T^2 : Toluene concentration of inlet flow at a temperature T (ppm).

Meanwhile, the conversion of Toluene into CO₂ was determined as equation 2

$$\gamma_{CO_2} = \frac{C_{CO_2,T}^2}{6(C_T^1 - C_T^2)} \times 100 \quad (2)$$

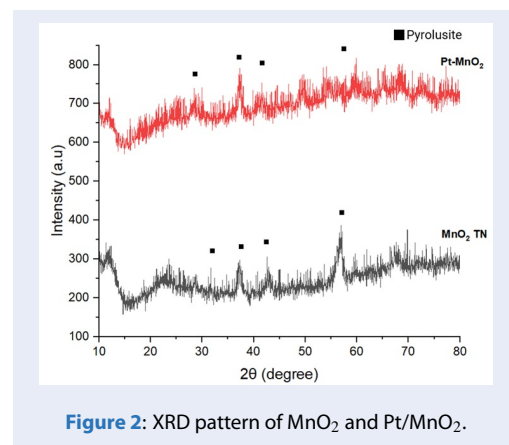
Whereas:

$C_{CO_2,T}^2$: CO₂ concentration of outlet flow at a temperature.

RESULTS AND DISCUSSION

Catalyst characterization

XRD spectroscopy was employed to examine the structural characteristics of the Pt/MnO₂ material. The XRD measurement findings for MnO₂ nanowire Pt/MnO₂ are shown in the following Figure 2.



Following the X-ray diffraction (XRD) characterization analysis, Pt peaks were not detected in the XRD

phase diagram. However, when Pt particles were introduced to the MnO₂ material, the intensity of the Manganese dioxide peaks decreased and became less distinct, as shown in the MnO₂ TN sample. Based on the XRD analysis, it is evident that the introduction of Pt metal onto MnO₂ does not induce any alterations in the phase structure of the material. This observation validates the complete preservation of the crystalline phase of MnO₂ while also indicating the uniform dispersion of Pt nanoparticles across the material's surface.

To further investigate the impact of the synthesis process on the creation of Pt/MnO₂ products, the synthesized sample underwent characterization using the Fourier Transform Infrared (FTIR) method throughout the wavelength range of 400 to 4000 cm⁻¹. The findings are presented in Figure 3.

Based on the Fourier Transform Infrared (FTIR) analysis of the two samples, it is evident that the introduction of Pt onto MnO₂ does not exert any discernible influence on the structural integrity of MnO₂. This is substantiated by the continued presence of the absorption band associated with Mn-O vibrations inside the MnO_x network, which remains observable within the wave number range of 400 ÷ 1100 cm⁻¹. The observed shift in the absorption peak of the Pt/MnO₂ sample towards a lower wavelength (503.38 cm⁻¹) in comparison to MnO₂ TN (456.41 cm⁻¹) might perhaps be attributed to the introduction of Pt into the [MnO₆] unit. This doping of Pt is likely to alter the vibrational frequency of the unit, consequently influencing both the intensity and position of the diffraction peak. The observed displacement of the FTIR spectrum following the introduction of Pt entirely agrees with the findings obtained from XRD analysis. The alignment of the Mn-O network in MnO₂ is notably impacted by the loading of Pt, resulting in deformation of the crystal lattice and a substantial reduction in the crystallinity of the sample. The oxygen exchange capacity of the catalyst is intricately linked to both its crystallinity and the number of defects present. The work conducted by Wang et al.⁹ demonstrated that the introduction of Pt loading induces deformation in the Mn-O lattice, resulting in an elevated presence of defects. This phenomenon facilitates the exchange of oxygen and consequently enhances the oxidation process. Therefore, noble metals could infiltrate the crystal lattice of the manganese oxide layer after the reaction, resulting in the creation of lattice imperfections and a decrease in the catalyst's crystallinity.

Meanwhile, The FTIR measurement in Figure 3b findings of Pt/MnO₂ samples with varying Pt loading

contents by mass % indicate a steady decrease in the strength of absorption peaks on the spectrum as the Pt loading content increases. The diagram still exhibits the typical absorption band of Mn-O, which is seen at wavelengths of 500 and 700 cm⁻¹. There is a positive correlation between the size of the loading content and the level of noise observed on the baseline. The synthesis of these samples with varying Pt loading amounts was successful, as evidenced by the absence of distinctive peaks corresponding to O-H groups in water and C=O of CO₂.

To examine the morphology of the Pt/MnO₂ material, the synthesized sample was subjected to observation using a scanning electron microscope (SEM). Figure 4 shows that upon Pt loading, the Pt/MnO₂ sample exhibits morphological features that closely resemble those of MnO₂ TN, except for the surface gaps occupied by sheet-shaped particles of varying sizes, ranging from 50 to 100 nm. The nanowire that remains detectable exhibits dimensions ranging from 200 to 600 nm.

The study employed the N₂ isothermal adsorption-release method to examine the impact of Pt loading on the surface of MnO₂, the result is shown in Figure 5 and Figure 6. The findings indicate that the adsorption-desorption pathway of the Pt/MnO₂ sample remains mostly unchanged when MnO₂ is loaded onto the surface of MnO₂. Furthermore, the Pt/MnO₂ sample continues to exhibit the complete features of the MnO₂ TN sample. The N₂ adsorption-release isotherms of both samples may be classified as class IV according to the IUPAC classification, which is particular for mesoporous materials. Additionally, the hysteresis curves are also indicative of this classification—the H₂ form. Capillary condensation occurs when the relative pressure (P/P₀) reaches approximately 0.9. The observed phenomenon can be attributed to the non-baked impregnation procedure, which little alters the material's surface. This outcome aligns entirely with the findings obtained by the scanning electron microscopy (SEM) measurement technique. Nevertheless, the introduction of Pt results in a marginal reduction in the specific surface area of the material. This drop can be attributed to the presence of Pt nanoparticles, which occupy a fraction of the voids on the MnO₂ surface.

The findings in Table 1 indicate that the specific surface areas of three samples, each with varying mass loading levels of Pt (0.5%w, 1%w, and 1.5%w, respectively), exhibit distinct relative surface areas. The specific surface area of the 0.5%Pt sample, as determined by the BET method, is measured to be 93.65 m²/g. Similarly, the specific surface area of the 1.5%w Pt

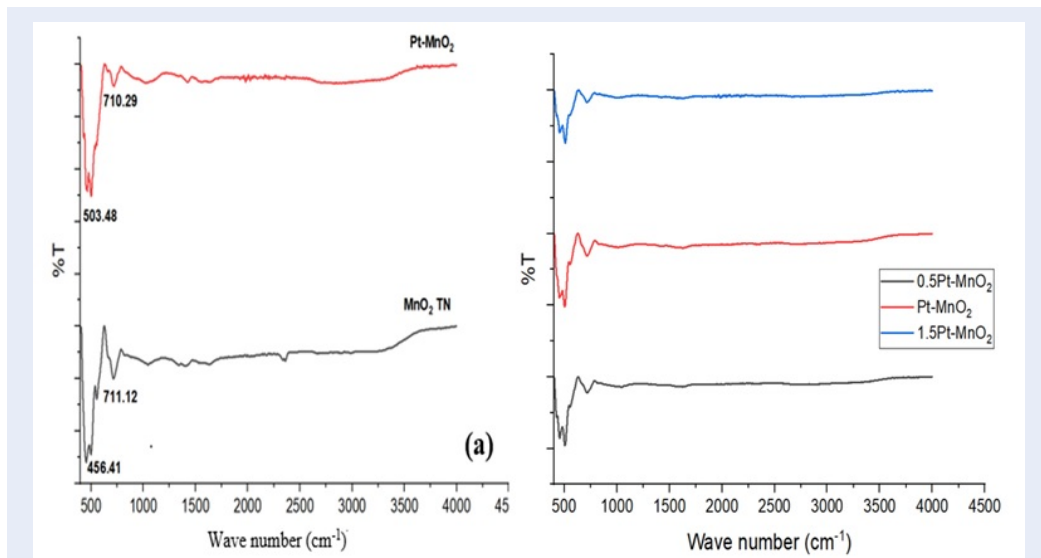


Figure 3: FTIR spectra of (a) Pt/MnO₂ and MnO₂ TN; (b) 0.5Pt/MnO₂, Pt/MnO₂, 1.5Pt/MnO₂

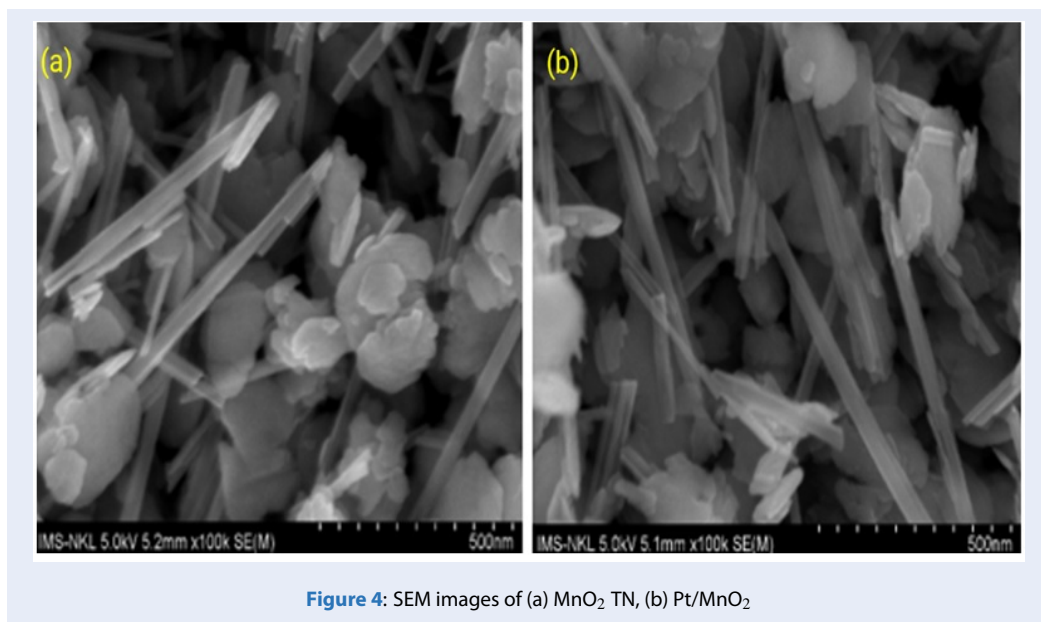


Figure 4: SEM images of (a) MnO₂ TN, (b) Pt/MnO₂

Table 1: Surface porous properties of all samples.

Sample	SBET (m ² /g)	dpore (nm)
MnO ₂ TN	113.7	25.76
0.5 Pt/MnO ₂	93.65	25.43
Pt/MnO ₂	108.74	24.88
1.5 Pt/MnO ₂	88.95	27.98

sample is 88.95 m²/g. Notably, the 1%w Pt sample exhibits the highest specific surface area among the three, measuring 108.74 m²/g.

The pore pattern seen in Figure 6 indicates the presence of medium and large capillaries in all three samples containing Pt. The sample containing 1% platinum exhibited the most significant proportion of pores ranging in diameter from 2 to 10 nanometers. The two remaining samples show comparable pore size distributions.

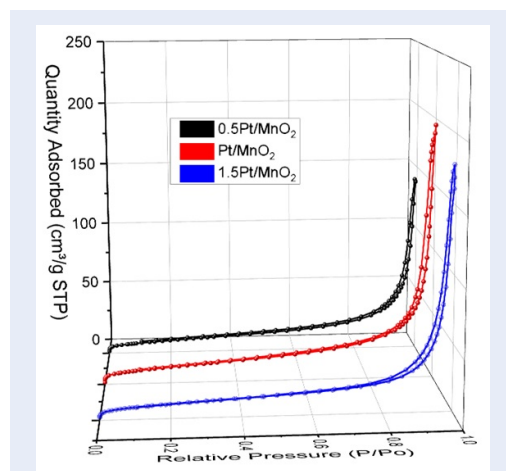


Figure 5: N₂ adsorption-desorption isotherms of all sample MnO₂

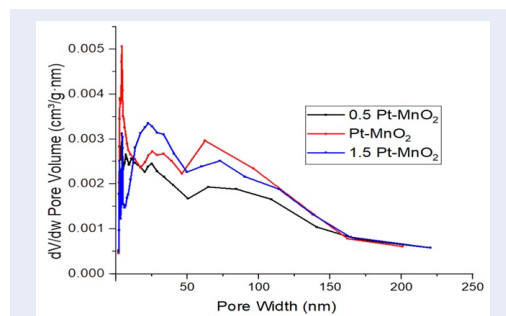


Figure 6: Capillary distribution curves of Pt/MnO₂ samples with different loading Pt contents

Energy Dispersive X-ray Spectroscopy (EDS) analysis on Table 2 reveals that the Pt content deposited on MnO₂ amounts to 1.01%, a value that closely aligns with the theoretical calculation. The platinum (Pt) content was uniformly distributed across the material's surface, maintaining a precise mass fraction of 1%. Regarding the MnO₂ TN sample, the analysis revealed the presence of peaks corresponding to the ele-

ments Mn and O. This suggests that the synthesis procedure effectively eliminated additional components, such as potassium (K) from KMnO₄ and sulfur (S) from MnSO₄, which were likely washed away during the sample preparation. The hydrothermal approach facilitates the synthesis of MnO₂ with a high degree of purity, devoid of any additional contaminants. Based on the observations above, it can be inferred that Pt was effectively transferred onto MnO₂, and the impregnation technique effectively facilitated the deposition of Pt particles onto the material's surface.

Catalytic activity

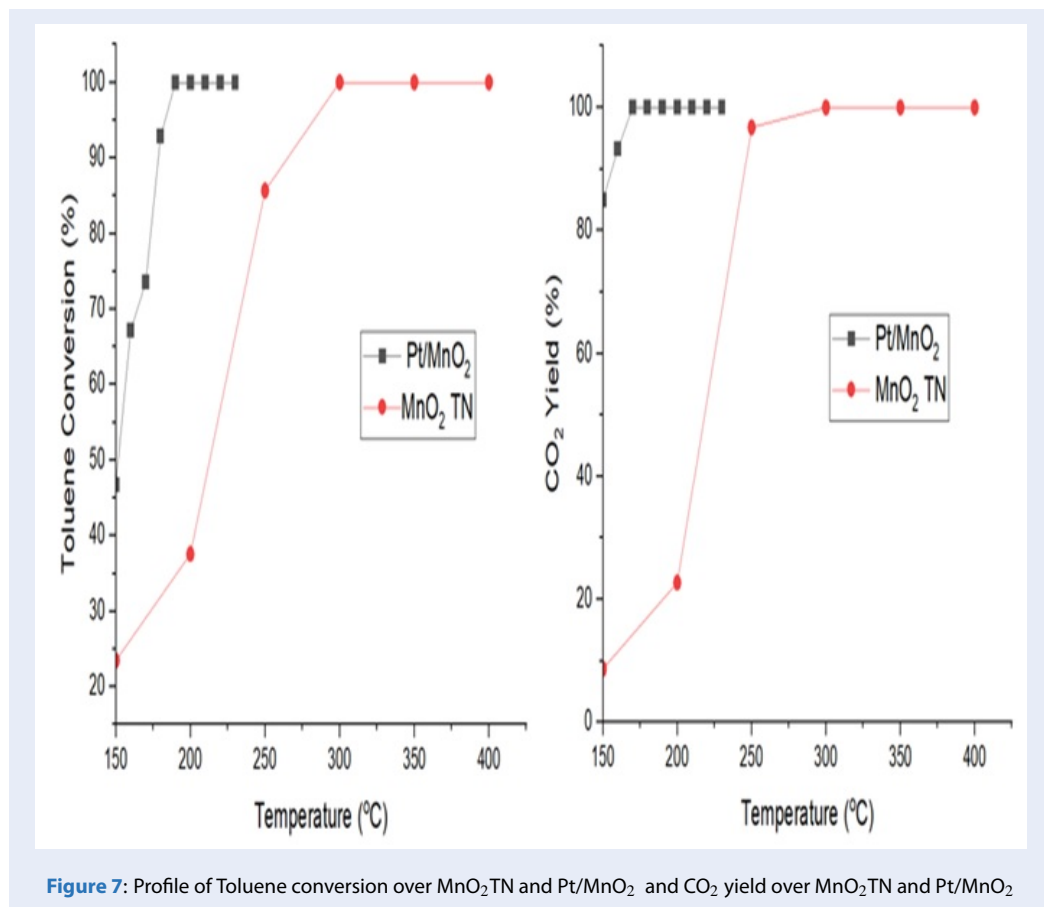
To examine the catalytic activity of the as-prepared catalysts, the toxic gas toluene was used as a model for catalytic oxidation. The experiments involved the complete oxidation of 6000 ppm of benzene vapor at a GHSV of 11000 h⁻¹. The results are illustrated in Figure 7.

Based on the conversion graph in Figure 7, it is evident that the utilization of Pt as a catalyst, despite its mere 1% mass loading, has led to a substantial enhancement in the conversion of the toluene oxidation reaction, surpassing the conventional transition metal oxide catalyst, such as Manganese oxide. When MnO₂ TN is present, it exhibits the capability to fully toluene convert at a temperature of 300 °C. However, by using a catalyst consisting of only 1% Pt by weight, the total conversion of toluene can be achieved at a significantly lower temperature of 190 °C. The graphs depicting the behavior of the two catalysts exhibit a high degree of similarity. This can be attributed to the fact that, during the initial stage, both catalysts primarily engage in the adsorption and oxidation of toluene, forming various intermediate molecules. The CO₂ selectivity of the MnO₂ TN catalyst sample showed a complete attainment of 100% at a temperature of 300 degrees Celsius. In contrast, the CO₂ selectivity of Pt/MnO₂ exhibited the ability to achieve a complete 100% selectivity starting from a lower temperature of 170 degrees Celsius. The results indicate that the Pt/MnO₂ catalyst effectively facilitated the extensive oxidation of toluene, resulting in the formation of less harmful byproducts such as CO₂ and H₂O, hence mitigating the occurrence of secondary pollution.

As we can see in Figure 8, the catalytic efficacy of manganese oxide is contingent upon various aspects, including the composition of oxygen within the network, the presence of vacant oxygen sites and adsorbed oxygen species, the surface area, and the oxidation state, among others. These factors exhibit a

Table 2: EDS analysis of MnO₂TN and Pt/MnO₂

MnO ₂ TN		
Element	Mass %	Atom %
O	43.36	72.44
Mn	56.64	27.56
Pt	-	-
Total	100.00	100.00
Pt/MnO ₂		
O	35.73±3.63	49.80±5.05
Mn	24.92±2.45	22.86±2.24
Pt	12.48±1.95	10.31±1.61
Total	100.00	100.00



strong correlation. The adsorption density of oxygen is positively correlated with the concentration of manganese in its high oxidation state (Mn^{4+}). Conversely, an increase in the quantity of manganese in its low oxidation state (Mn^{2+}) leads to an increase in the density of oxygen vacancies. The impact of oxidation state distribution on the catalytic activity of manganese oxide has been demonstrated by Tang et al.³⁶ Specifically, the ratio of $\text{Mn}^{2+}/\text{Mn}^{4+}$ has been identified as a crucial factor influencing the material's catalytic activity. The author has demonstrated that manganese oxide displays optimal activity when the ratio of $\text{Mn}^{2+}/\text{Mn}^{4+}$ approaches unity. The redox mechanism plays a crucial role in the oxidation of BTX on manganese oxide $\text{Mn}^{4+} \leftrightarrow \text{Mn}^{3+} \leftrightarrow \text{Mn}^{2+}$ at this particular ratio, facilitating a smooth reaction. Consequently, introducing Pt onto the catalyst surface induces robust metal support interactions between noble metals and metal oxide support materials, enhancing catalytic performance. Sengpeng et al.³⁷ made evidence in their study that including Pt on the surface of MnO_2 decreases the links between Mn and O atoms, hence enhancing the mobility of oxygen within the network. The presence of crystals on the catalyst surface can facilitate the efficient oxidation of toluene, even at very moderate temperatures. This phenomenon may explain the substantial disparity observed in the conversion rate.

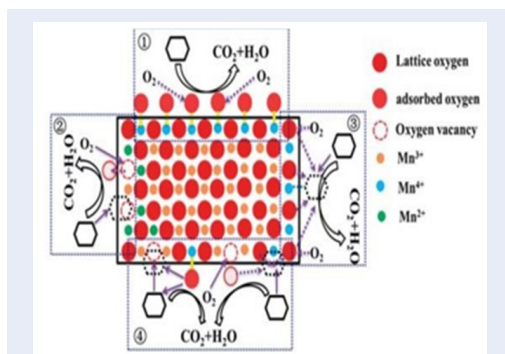


Figure 8: Possible mechanism with oxidation reaction on manganese oxide

A set of experiments was performed on a microflow system to evaluate the efficacy of the catalysts. The system had a total gas flow rate of 60 ml/min and a volume rate of 11000 h^{-1} . The specimens were placed at the midpoint of the reaction tube, each weighing 0.1 gram, and subjected to a toluene treatment with a concentration of 9000 ppm. Figure 9 displays the outcomes of an investigation into the catalytic activity

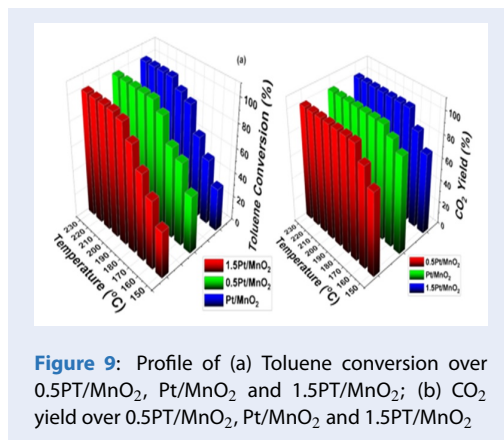


Figure 9: Profile of (a) Toluene conversion over 0.5Pt/MnO₂, Pt/MnO₂ and 1.5Pt/MnO₂; (b) CO₂ yield over 0.5Pt/MnO₂, Pt/MnO₂ and 1.5Pt/MnO₂

of Pt/MnO₂ samples with varying Pt concentrations in the process of toluene oxidation.

Based on the findings derived from the analysis of catalytic activity in the microflow system, as depicted in Figure 9, it is evident that the conversion efficiency of the examined samples exhibits a progressive increase in the following sequence: $1.5\text{Pt}/\text{MnO}_2 < 0.5\text{Pt}/\text{MnO}_2 < \text{Pt}/\text{MnO}_2$. This outcome can be elucidated in full accordance with the findings of the distinctive measuring experiments done. The Pt/MnO₂ sample possesses a crystalline structure characterized by the presence of rods and particles, which contributes to its substantial specific surface area and notable porosity. Consequently, this structural configuration enhances the catalyst's ability to adsorb oxygen and toluene on its surface, facilitating these substances' absorption. The Pt/MnO₂ catalyst model has enhanced efficacy in facilitating the oxidation process of toluene. It demonstrates the capability to achieve complete conversion of toluene at a temperature of 190 °C, while also attaining a CO₂ selectivity of 100% at 170 °C.

A series of tests were conducted to investigate the catalytic stability, including a catalytic activity test conducted at a temperature of 190 °C. However, it is worth noting that during this test, the catalyst was subjected to continuous testing for a duration of 10 hours.

Based on the findings of the catalytic durability investigation, it is evident from Figure 10 that the Pt/MnO₂ catalyst required an initial stabilization period of 50 minutes. During the initial phase of the reaction, the conversion rate ranges from 88% to 96%. This is mainly attributed to the adsorption of toluene and oxygen from the gas stream onto the surface. However, the quantity of oxygen adsorbed remains insufficient for the complete oxidation of toluene. The CO₂

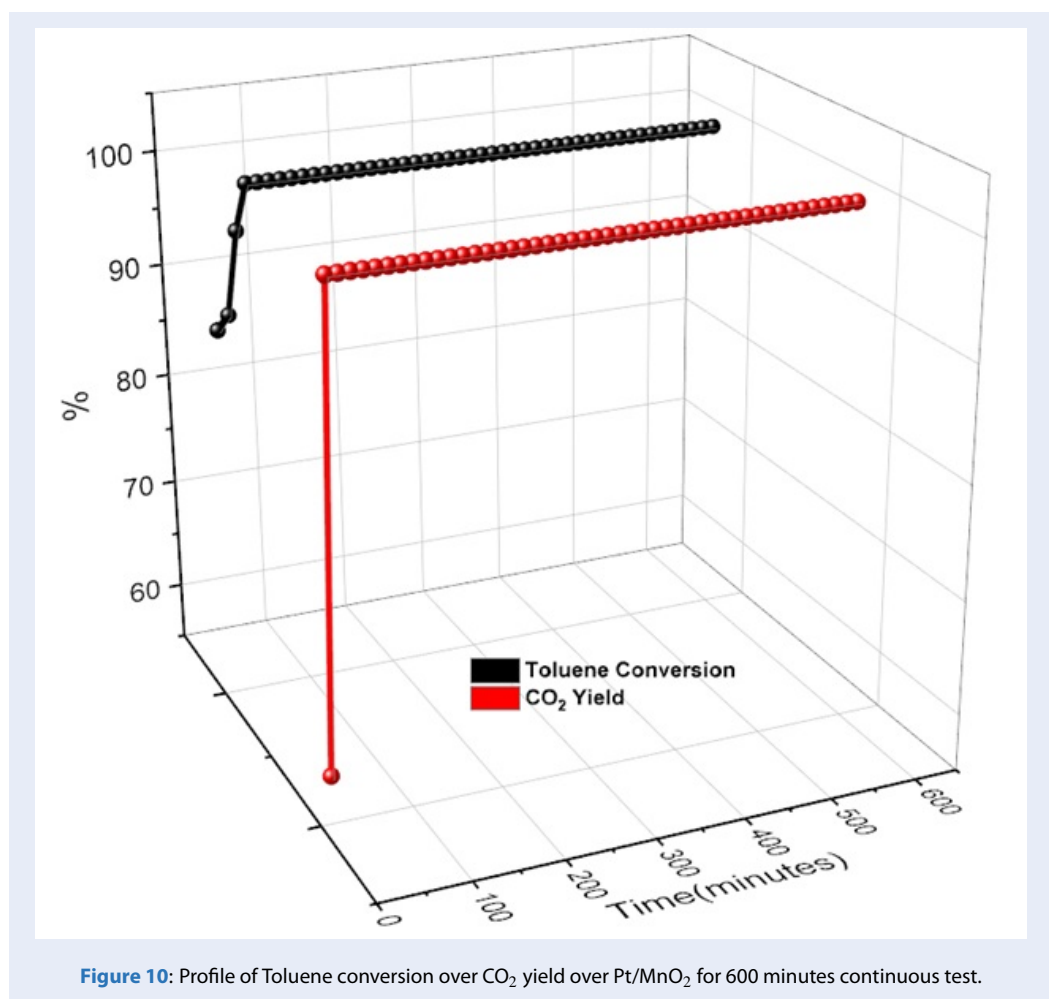


Figure 10: Profile of Toluene conversion over CO₂ yield over Pt/MnO₂ for 600 minutes continuous test.

selectivity graph reveals a notable trend during the initial 12.75-minute interval. Specifically, the CO₂ selectivity is noted to be merely 60%, while the toluene conversion attains a significantly higher value of 88%. This indicates that the majority of the toluene is primarily digested. The primary factor contributing to this phenomenon is the adsorption process occurring on the surface, coupled with oxidation. However, it is essential to note that this process yields intermediate products rather than complete oxidation, producing CO₂ and H₂O. Throughout the duration spanning from 50 minutes to 10 hours, the conversion and selectivity of CO₂ remained consistently high at 100%. Notably, no discernible variations were seen during the activity test. The Pt/MnO₂ catalyst has commendable characteristics and demonstrates notable temperature stability. Due to the relatively mild reaction conditions maintained at a temperature of 190 °C, there remains a lack of observable indications pertaining to the sintering or clustering of Pt particles. Conse-

quently, the catalytic activity of the catalyst is minimally impacted.

CONCLUSION

To assess the catalytic efficacy of platinum in conjunction with manganese oxide, a range of Pt/MnO₂ samples with varying mass fractions of platinum were synthesized, described, and subjected to testing for the complete oxidation of toluene. The Pt/MnO₂ catalyst containing one wt% of platinum exhibited superior catalytic performance compared to the toluene oxidation activity in the other samples. Additionally, it shows the most significant surface area. The active phase for toluene oxidation in Pt/MnO₂ was determined to be Pt. The robust interaction between the noble metal platinum (Pt) and manganese oxide (MnO₂) contributes to the enhanced stability of the Pt/MnO₂ oxide catalyst during oxidation processes.

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LIST OF ABBREVIATIONS

Ppm: point per million
 GHSV: Gas hourly space velocity
 VOCs: volatile organic compounds

CONFLICT OF INTERESTS STATEMENT

The authors want to make sure that there is no conflict of interest in the article's publication.

CREDIT AUTHORSHIP CONTRIBUTION STATEMENT

Tran Van Hien: Conceptualization, Validation, Supervision, Project administration, Funding acquisition.

Ha Quoc Bang: Conceptualization, Methodology, Validation, Supervision, Writing – review & editing

Khong Manh Hung: Methodology, Data curation, Formal analysis, Resources, Investigation, Writing – review & editing.

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Xúc tác trên MnO_2 được kết hợp Pt để cải thiện quá trình oxy hóa VOCs

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TÓM TẮT

Một trong những nguyên nhân hàng đầu gây ô nhiễm không khí đó chính là các hợp chất hữu cơ dễ bay hơi (VOCs), các hợp chất này không những gây nguy hiểm nghiêm trọng cho môi trường mà còn ảnh hưởng sức khỏe con người. Quá trình oxy hóa xúc tác đã được công nhận là một phương pháp đầy hứa hẹn và thành công để xử lý VOC. Do giá cả phải chăng và tính thân thiện với môi trường, oxit gốc mangan là một trong những lựa chọn không thể bỏ qua để phân hủy VOCs bằng xúc tác. Trong nghiên cứu này, chúng tôi phân tán Pt trên MnO_2 với hàm lượng về khối lượng của Pt lần lượt là 0,5, 1 và 1,5% để kiểm soát sự tương tác của Pt- MnO_2 . So với MnO_2 , chất xúc tác Pt- MnO_2 thể hiện hiệu suất oxy hóa VOC cao hơn do diện tích bề mặt Brunauer-Emmett-Teller cao, oxy mangan hoạt động mạnh hơn, các nguyên tử Pt tiếp xúc nhiều hơn. Trong số tất cả các mẫu thực vật được tạo ra với tỷ lệ khối lượng khác nhau, mẫu Pt- MnO_2 thể hiện các đặc tính cũng như hoạt tính xúc tác tốt nhất. Diện tích bề mặt riêng của Pt- MnO_2 là 108,74 m²/g. Chất xúc tác Pt- MnO_2 có thể chuyển đổi hoàn toàn Toluene thành CO₂ và H₂O ở nhiệt độ thấp hơn chỉ 190 C mà vẫn duy trì độ ổn định cao trong 600 phút. Trong điều kiện tốc độ không gian cao, hiệu suất của chất xúc tác Pt- MnO_2 trong quá trình oxy hóa VOC tương đối ổn định, cho thấy triển vọng to lớn khi sử dụng trong thực tiễn. Nghiên cứu này cho thấy chất xúc tác MnO_2 phân tán Pt vượt trội hơn chất xúc tác MnO_2 thông thường trong quá trình oxy hóa VOCs.

Từ khóa: Mangan oxit, Bạch kim, Toluen, Oxi hóa xúc tác, VOCs

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